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Design, Build, and Analyze: A Comprehensive Approach to Developing a Thermal Dehydrator Prototype

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Abstract: Fruit and vegetable preservation commonly relies on drying methods, and dehydrators play a pivotal role in enhancing traditional sun-drying processes. This report delves into the intricate calculation and analysis of a specific household electric dehydrator model with a 5kg capacity. Employing a meticulously chosen 5 kg sample of grapes with an initial 80% w.b(wet basis) moisture content, the dehydrator was analysed at temperatures of 45, 50, and 60 degrees Celsius.

The study scrutinizes the technical nuances of the electric dehydrator, aiming to provide a comprehensive understanding of its performance. By meticulously detailing the calculations and outcomes, this report contributes valuable insights into the efficiency of the dehydrator model, offering a foundation for future applications in fruit and vegetable preservation technologies.

Keywords: Film coefficient, Conjugate Heat Transfer (CHT) Analysis

I. INTRODUCTION

Vegetables and fruits are not mere components of our diet; they stand as pillars of global agricultural food production and, more critically, as agents of health promotion and disease prevention. Numerous medical studies underscore their role in providing essential phytonutrients and bioactive compounds necessary for optimal health. The diverse array of nutrients, including phenols, polyphenols, vitamin E, ascorbic acid, phytoestrogens, flavonoids, isoflavones, terpenes, lignans, lycopene, and biotin, collectively contribute to a balanced and healthful diet. Despite being the world's second-largest harvester of vegetables and fruits, India faces a paradox—15% of the population goes hungry daily, around 23 crore people live below the poverty line, and 1 in 4 children is malnourished. Approximately 3000 lives are lost each day due to illnesses resulting from poor dietary choices.

One glaring challenge contributing to this paradox is the irregular availability of fresh produce throughout the year. The Portable Vegetable Dehydrator project seeks to address this issue by harnessing the power of dehydration—a time-tested and traditional postharvest method. By stabilizing and extending the shelf life of vegetables, dehydration ensures a consistent and cost-effective addition to the diet, irrespective of the season. Traditional drying methods, often conducted in open spaces, are not without drawbacks—hygiene concerns, contamination, temperature inconsistencies, and space requirements are persistent challenges. The proposed dehydrator aims to overcome these limitations by offering a portable solution with adjustable temperature settings, time controls, and an efficient tray system that maximizes capacity while minimizing space requirements. The incorporation of features such as removable trays with mesh and vents, coupled with an exhaust fan for moisture removal, ensures effective and hygienic drying.

In essence, the Portable Vegetable Dehydrator endeavors to revolutionize the traditional methods of drying fruits and vegetables, presenting an innovative solution to address issues of storage, spoilage, and cost-effectiveness throughout the year, contributing towards a more sustainable and nourished future.

II. LITERATURE REVIEW

Dehydration is a common method of preserving vegetables, as it can extend their shelf life and retain their nutritional value. Here is a literature review on dehydration of vegetables.

1) *Dehydration of vegetables: a review* - K. J. Kadam and S. S. Salunkhe (1998)

This comprehensive review article provides an overview of the dehydration process, including factors affecting dehydration, methods of dehydration, and quality considerations. The article also discusses the nutritional aspects of dehydrated vegetables and their potential health benefits.

2) *Nutritional quality of dehydrated vegetables - M. J. Ayala-Aponte, et al. (2017)*

This study evaluated the nutritional quality of dehydrated vegetables, including carrots, sweet potatoes, and bell peppers. The researchers found that dehydrated vegetables retained most of their nutrients, including vitamins, minerals, and fiber. They concluded that dehydrated vegetables could be a good source of nutrients in diets.

3) *Drying of vegetables by heat pump: a review - S. Y. Al-Zuhair and I. M. Al-Harashsheh (2009)*

This review article focuses on the use of heat pump drying for vegetables. The authors discuss the advantages of this method, such as reduced energy consumption and improved product quality. They also provide an overview of the process and discuss the factors that affect the drying rate.

4) *Effect of pre-treatment on drying kinetics and quality of dehydrated vegetables - P. V. Shah and S. L. Sonawane (2014)*

This study evaluated the effect of pre-treatment methods, such as blanching and chemical treatment, on the drying kinetics and quality of dehydrated vegetables. The researchers found that pre-treatment significantly affected the drying rate and the quality of the dehydrated vegetables. They recommended that pre-treatment should be optimized to achieve the desired quality.

5) *Optimization of microwave dehydration conditions for carrot cubes using response surface methodology - M. A. Dehghani and M. R. Omid (2018)*

This study used response surface methodology to optimize the microwave dehydration conditions for carrot cubes. The researchers found that the optimal conditions for microwave dehydration were a microwave power of 450 W, a sample thickness of 5 mm, and a dehydration time of 6 min. They also found that microwave dehydration retained the quality and nutritional value of the carrots.

6) *Recent Advances in Drying and Dehydration of Fruits and Vegetables: A review. Sagar V. R. Suresh Kumar P. J Food Science Technol. Jan-Feb. 2010.*

The paper discusses the challenges of traditional drying methods for fruits and vegetables and explores advanced techniques such as osmotic dehydration, vacuum drying, and freeze drying. Emphasizing the importance of energy efficiency and product quality, the review underscores the need for cost-effective and sustainable drying processes in post-harvest management.

III. DESIGN AND MANUFACTURING

During designing process, the size and the shape of the prototype was taken into consideration. The main aim was to make the portable as well as the aesthetically pleasant. To minimise the shape used by the product is designed to be the square in shape and 2 trays are stacker inside it.

The drying compartment was constructed from plywood (10 mm thickness) coated with an insulating foil having the 0.1mm thickness and dimensions same as prototype dehydrator.. Three trays with stainless steel mesh were provided inside the drying chamber for loading the sample. The dryer is equipped with heating element (12 V), an axial flow fan (85 CFM), thermostat (range: 25C-80C)

Sr. No	Component Name	Specification
1	Plywood	10 mm thick
2	Insulating Foil	0.1mm thick
3	Heating Element	12 V
4	Axial Flow Fan	85 CFM
5	Thermostat	Range 25C- 80 C

IV. WORKING OF DEHYDRATOR

In the operational context, the dehydrator operates on the principles of forced convection and drying, constituting a complex interplay of heat and mass transfer processes. The heat transfer occurs through forced convection, where the heating coil, when activated, elevates the air temperature within the dehydrator to the specified drying temperature of the material. Simultaneously, the fan facilitates the circulation of heated air over the material on the drying trays, promoting the transfer of heat from the air-food interface.

This convective heat transfer process is integral to the dehydration mechanism, wherein water diffuses from the interior of the food material to the air-food interface and is subsequently carried away by the convecting air stream. The vents strategically placed at the dehydrator's end serve as outlets, allowing moist air to escape, thereby aiding in the overall drying process.

For analysis purposes, the study focused on the fundamental principles of heat transfer through convection, assuming a constant air flow and temperature during the process. The dehydrator continues its operation until a consistent weight of the sample is achieved, indicating the completion of the dehydration process. This systematic approach ensures effective dehydration of the sample within the specified parameters.

V. METHODOLOGY

In the methodology, a 5kg sample of grapes with an initial moisture content of 80% underwent analysis. The drying process aimed to achieve a moisture content of 18% at a drying temperature of 60°C over a period of 40 hours.

The analysis commenced by calculating the dry matter weight, determining the amount of water to be removed. Subsequently, the heat energy and power required for water evaporation were computed. This involved the calculation of the heat transfer rate of the dryer and the coefficient of thermal conductivity.

To delve deeper, two key terms were introduced: Wet Basis and Dry Basis Moisture Content. Wet Basis Moisture content (M_w) was defined as the percentage ratio of water weight (W_w) to the total material weight (W_i). On the other hand, Dry Basis Moisture Content (M_a) represented the percentage ratio of water weight (W_w) to the weight of dry matter (W_a). Dry Basis moisture content is commonly used in describing moisture changes during drying processes.

The methodology also included the calculation of film coefficient and associated factors like the Nusselt number. Subsequently, thermal analysis was conducted using ANSYS to comprehensively understand the heat transfer dynamics during the dehydration process. This multifaceted approach ensures a thorough investigation into the thermal aspects of the grape dehydration, encompassing both theoretical calculations and practical simulations.

VI. CALCULATIONS

A. Dry Matter Weight (D_m)

$$D_m = W_m - (W_m * M_{ciw}/100)$$

$$D_m = 1 \text{ kg}$$

Where,

W_m = Weight of grapes = 5kg

M_{ciw} = Initial moisture content of grapes (before drying) wet basis % = 80%

B. Initial Moisture Content Dry basis – before drying (M_{cid})

$$M_{cid} = M_{ciw}/(100 - M_{ciw})$$

$$M_{cid} = 4\%$$

C. Final Moisture Content Dry Basis – After Drying (M_{cfd})

$$M_{cfd} = M_{cfw} / (100 - M_{cfw})$$

$$M_{cfd} = 0.25\%$$

Where,

M_{cfw} = Moisture content of grapes (after drying) wet basis % = 18 %

D. Mass of Water to be Removed (M_r)

$$M_r = [(M_{cid} - M_{cfd})/100] * D_m$$

$$M_r = 3.75 \text{ kg}$$

E. Quantity of heat needed to evaporate the water(H)

$$H = Wm * Cc *(T2 - T1)$$

$$H = 581.9275 KJ$$

$$= 581927.5 J$$

Where,

Cc = Specific Heat Capacity of Grapes = 3.3253 KJ/Kg C

T1 = Initial temperature of cabinet (Room temperature)

T2 = Drying temperature of Grapes as specified

F. Power Required to Evaporate water (Hz)

$$Hz = H/3600$$

$$Hz = 161.64 KJ/h$$

G. Convective Heat Transfer Coefficient (h)

$$h = Nu * k / D$$

$$h = 7.399 W/m^2. K$$

Where,

Nu = Nusselt Number = 121.3 = 0.13 Ra ^{0.33}

Ra = Rayleigh Number = 10⁹

k = Thermal Conductivity (w/m.k)

D = Hydraulic Diameter

H. Heat Transfer Rate (Qr)

$$Qr = A * h * (T2 - T1)$$

$$Qr = 42.7 KJ$$

Where,

A = Area of dryer = 0.165 m²

h = Convective Heat Transfer Coefficient = 7.399 W/ m².k

T1 = Initial temperature of cabinet (Room temperature)

T2 = Drying temperature of Grapes as specified

I. Drying Rate of the Dryer (RD)

$$RD = (wi - I) - wf / 100(Tf - I) - ti$$

$$RD = 0.000769 Kg / h$$

Wi = Initial Weight of Grapes = 5 kg

Wf = Final Weight of Grapes = 1 kg

Tf = Time after drying or time needed to dry = 40h

Ti = Initial time = 0 h

J. Air Flow Rate (Qa)

$$Qa = [(pi * d) / 60] * N$$

$$Qa = 2.61 m/s$$

Where ,

d = Diameter of fan blade = 0.05 m

N = Rpm of the fan = 1000 rpm

K. Drying Efficiency (nd)

$$nd = [Hz/(Qr*T)] * 100$$

$$nd = 86.6 \%$$

Hz = Power Required to evaporate water= 161364 KJ/ h

Qr = Heat Transfer Rate = 42.7 KJ

T = Time required to dry = 40h

VII. CAD MODEL

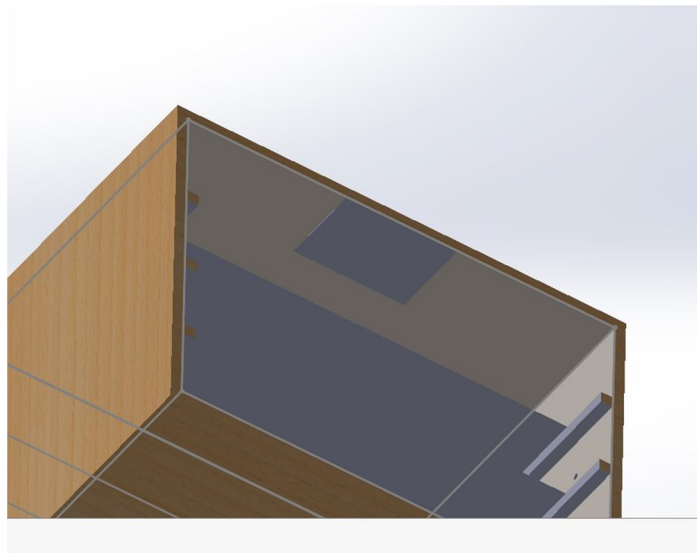


Fig. 1. CAD Model of Prototype Dehydrator

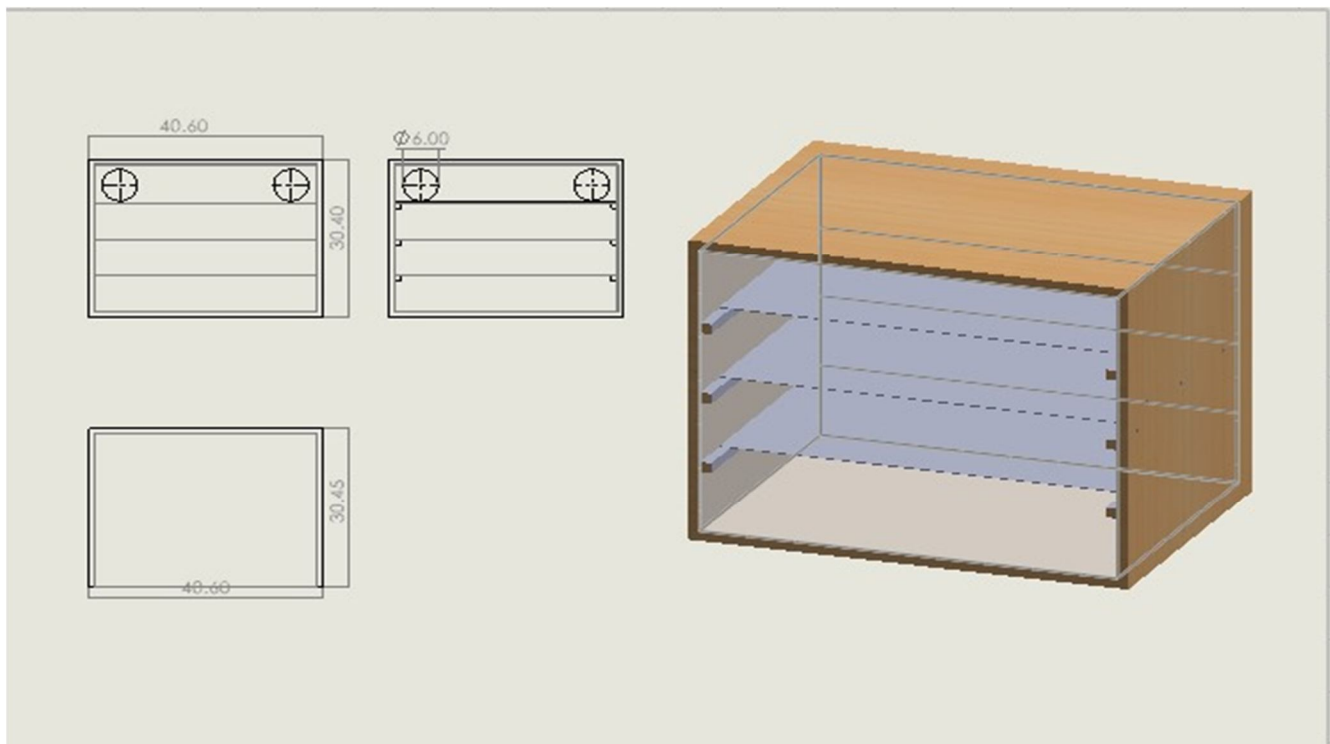


Fig. 2. Dimensions of the prototype (The main box)

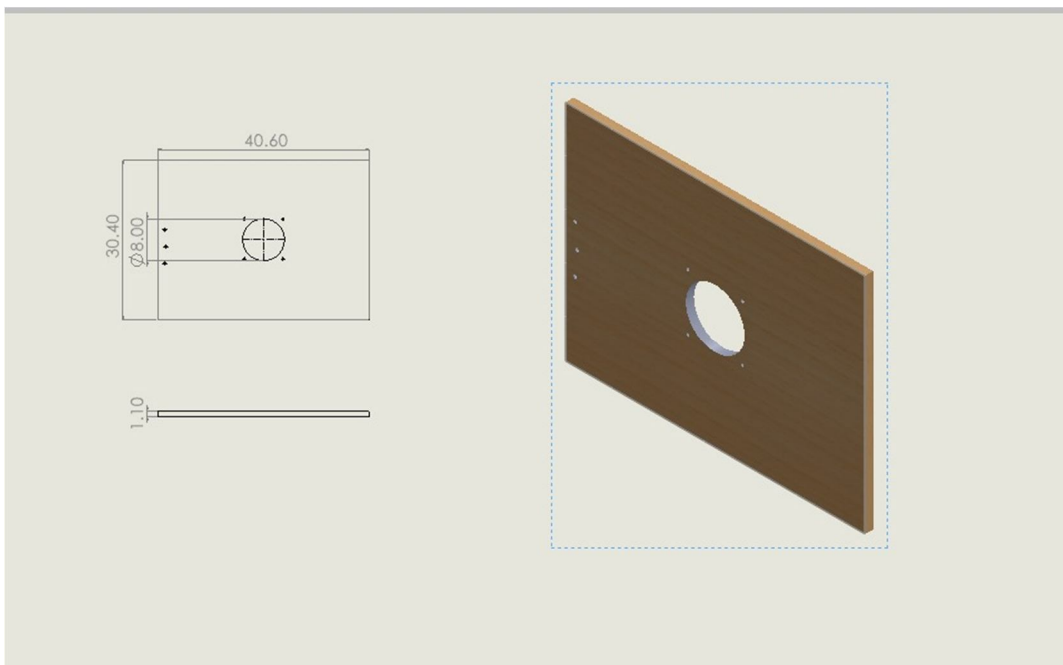


Fig. 3. Dimensions of the prototype (The gate)

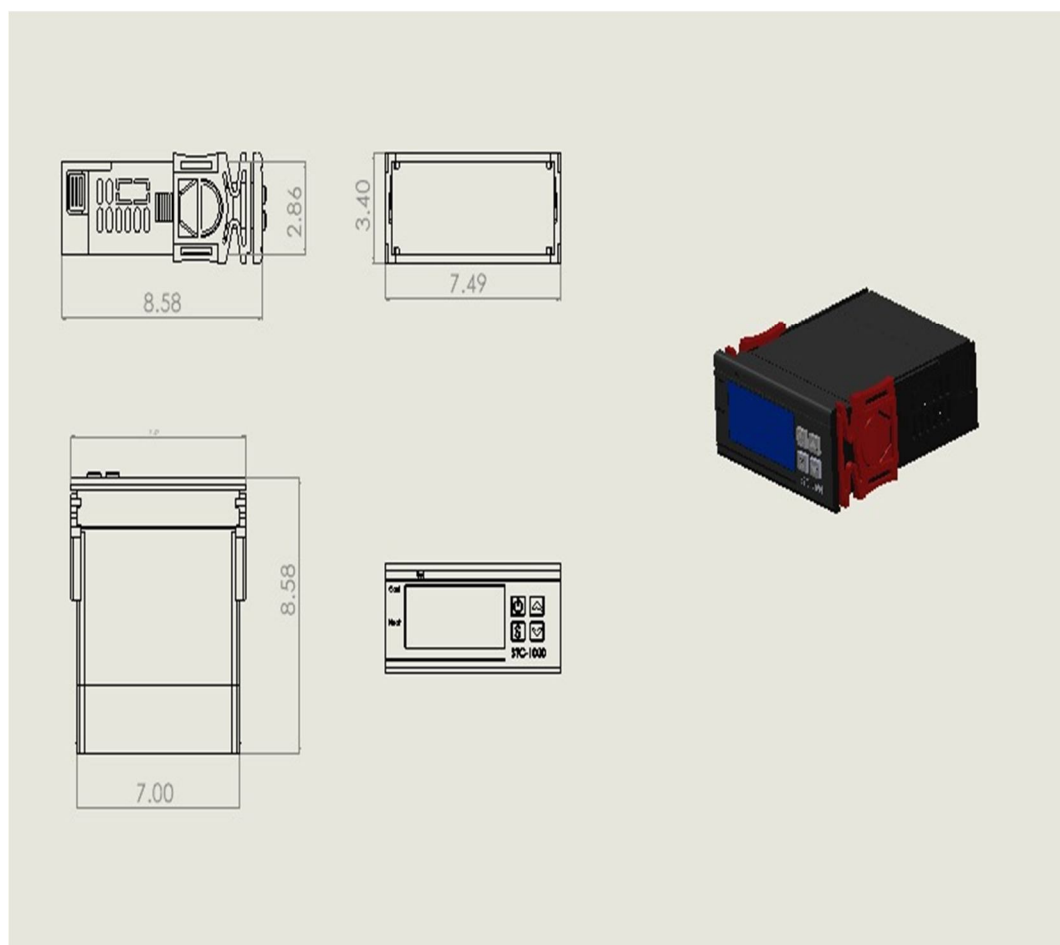


Fig. 4. Dimensions of Thermostat

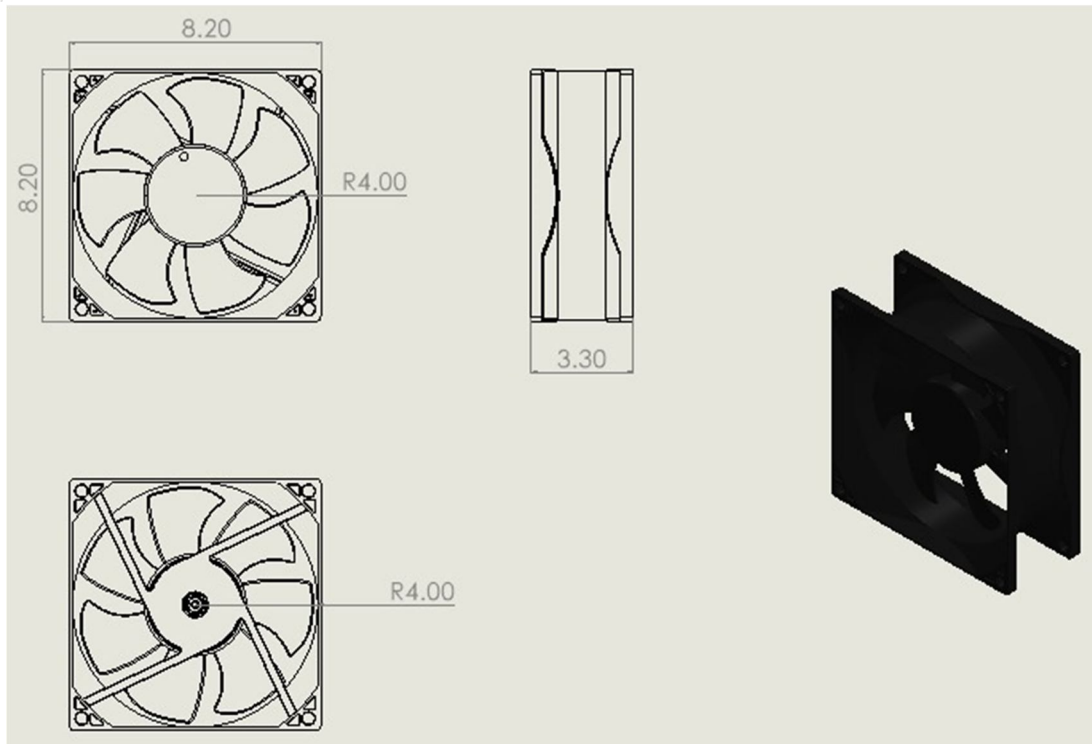


Fig. 5. Dimensions of Fan

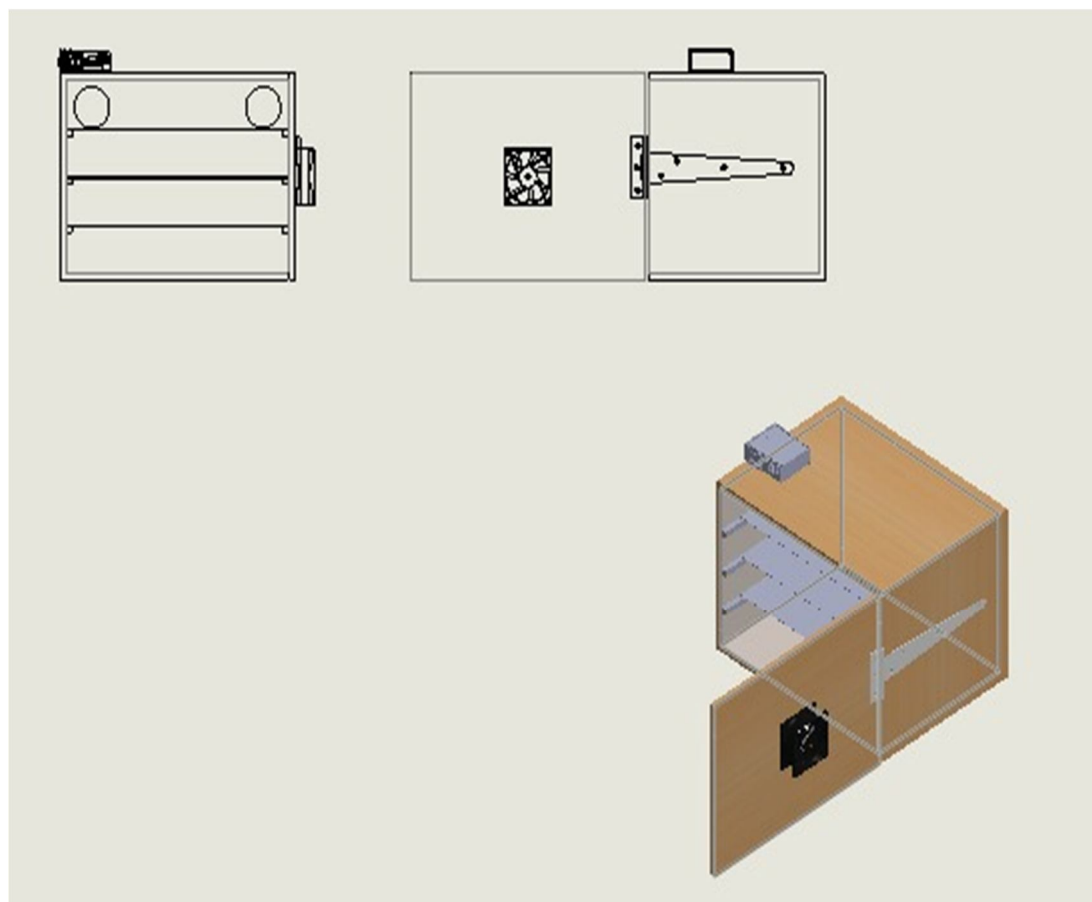


Fig. 6. Prototype CAD Model

VIII. RESULTS OF THERMAL ANALYSIS

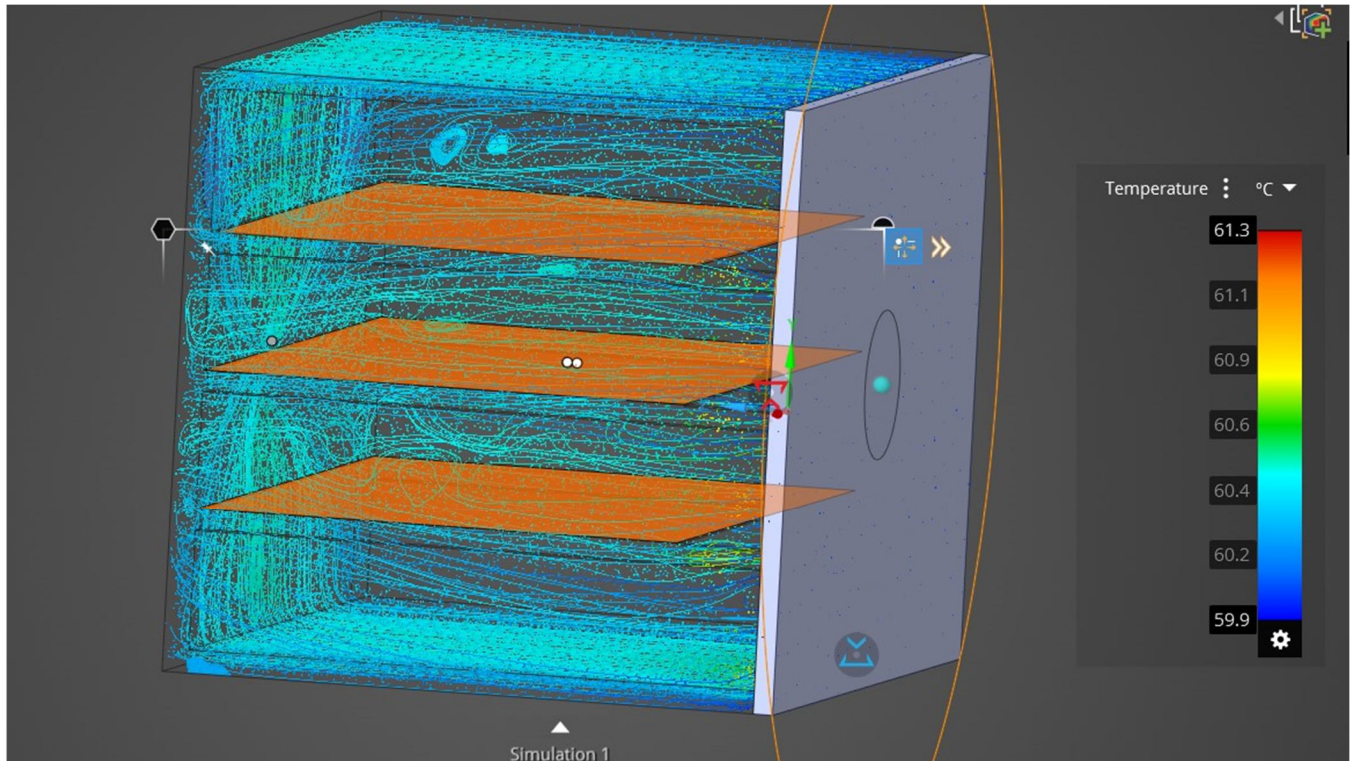


Fig. 7. Temperature Gradient

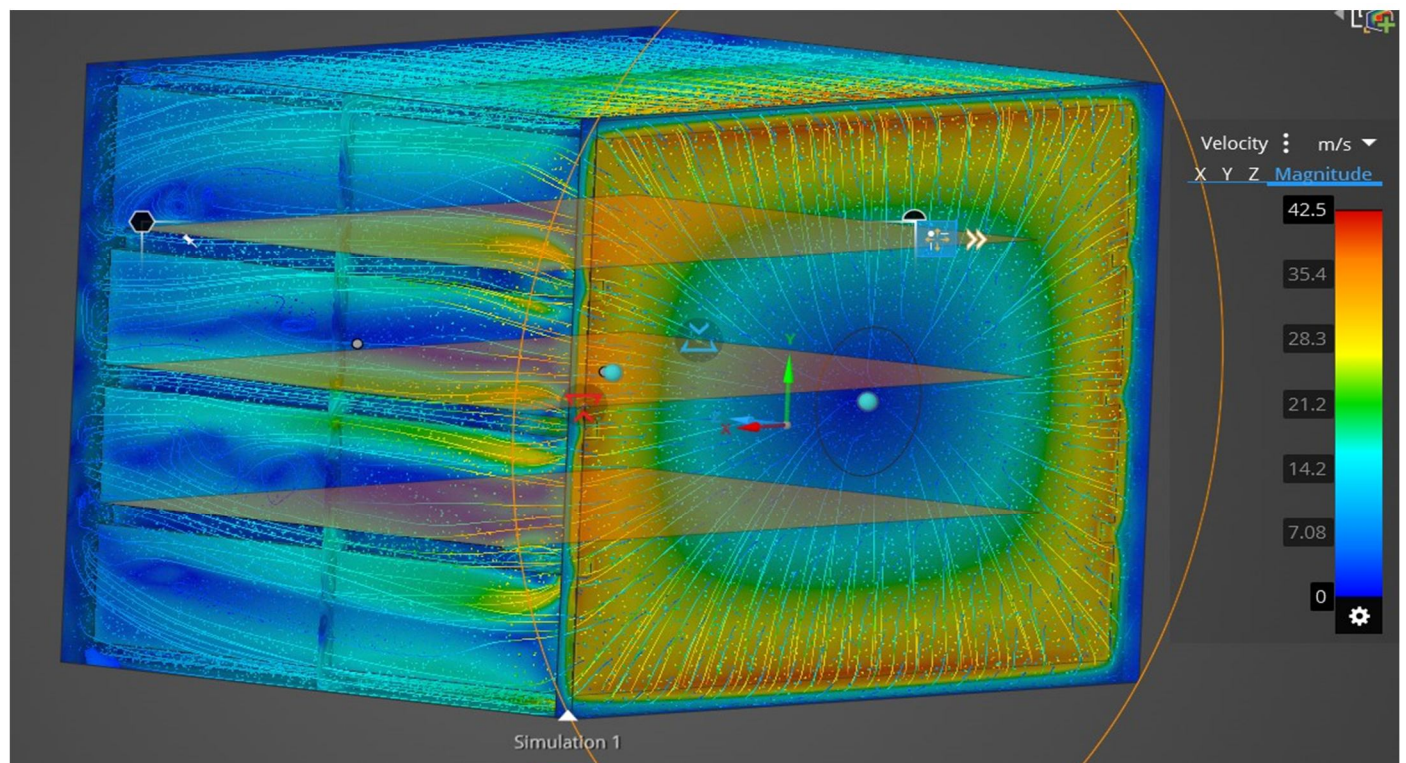


Fig. 8. Velocity Gradient

XI. CONCLUSION

In conclusion, the exhaustive thermal analysis conducted on the fruit dehydrator unveils a project marked by meticulous design and impressive efficiency. The uniform temperature distribution, characterized by a minimal variation of less than 2°C, speaks to the precision embedded in the dehydrator's construction. This critical feature ensures a consistent and thorough drying process for an array of fruits, affirming the practicality and versatility of the equipment.

The effectiveness of the drying process is a standout aspect, with the dehydrator demonstrating its ability to reduce moisture content to below 10% within a relatively brief duration. This not only attests to its efficiency but also positions the equipment as a practical solution for both domestic and commercial fruit drying needs.

Beyond the technical achievements, the dehydrator's user-friendly interface and straightforward maintenance add a layer of practicality and accessibility. The simplicity of controls, coupled with ease of cleaning, contributes to the overall user experience and makes the equipment adaptable to a diverse user base.

In essence, this project represents a harmonious amalgamation of theoretical knowledge and practical application. The fruit dehydrator, emerging from this endeavor, stands as a testament to thoughtful engineering, efficient functionality, and user-centric design. It not only advances our understanding of heat transfer dynamics in the context of dehydration but also presents a tangible solution that bridges the gap between theory and real-world application in the realm of food processing technology.

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