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# Sulphonated PEEK-Azadirachta indica based Composite Membranes for PEM Fuelcells

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**Abstract:** Sulphonated Poly Ether Ether Ketone (SPEEK) – Azadirachta indica (AI) composite membranes have been prepared by varying AI from 0%, 1%, 2%, 3%, 4% and 5% while varying polymer content 100%, 99%, 98%, 97%, 96% and 95% by solution casting technique at 80°C environment. The obtained films were subjected to Ion Exchange Capacity (IEC), Water Absorption (WA), Chemical Stability (CS), Protonic Conductivity (PC) with view to understand the compatibility for their utility in PEM Fuel cell application. AI5 (SPEEK 95wt% + AI 5wt%) has maximum IEC, maximum WA, and minimum CS compared to pure SPEEK. The conductivity studies on the six selected samples show the maximum conductivity is noted for AI5. This may be reasoned that maximum WA with enhanced IEC only paved the way for good protonic transport mechanism. The FTIR studies confirms the Sulphonation of PEEK and complexation of SPEEK with AI. SEM shows the surface morphology of pure SPEEK and SPEEK/AI composite membranes, It is observed that beyond 5 weight% dispersion in SPEEK matrix, no free standing membrane is obtained which may be due to immiscibility of AI with SPEEK. Thus AI5 is the maximum dispersion of wood in SPEEK in the form of white patches and is found to be a critically compatible and viable membrane. XRD studies on PEEK, SPEEK, AI powder and SPEEK/AI composite membranes showed the transformation of semi-crystalline PEEK into amorphous membrane as part of introduction of SO<sub>3</sub> by sulphonation and making composite with AI. TGA studies confirms the sulphonation by the three step degradation as weight loss shown and ensured the membrane suitability to be used as PEM for PEMFC as there is no significant weight loss up to 230 °C and for PEMFC the operational temperature is very well below that. MEA prepared with pure SPEEK as well as SPEEK/AI5 membranes and subjected to realtime PEMFC testing which resulted in better OCV as well as power density.

**Keywords:** Polymer Electrolyte Membrane Fuelcell, SPEEK+AI composite, Proton conductivity, Water Absorption, Realtime PEMFC test

## I. INTRODUCTION

The rapid reduction of fossil fuels and hazardous impact of greenhouse gases on the environment exerts compulsion on the extensive research and development on alternative energy systems. The proton exchange membrane fuel cell (PEMFC) is an electrochemical energy device which has an advantage of converting chemical energy directly into electrical energy with high efficiency. It is considered to be a promising technology for future portable appliances including transportation [1-4]. The proton exchange membrane (PEM) is the key compartments of a PEMFC, PEM plays different roles in a fuelcell which includes proton transfer and separating reactant gases from each other. Presently Nafion (Dupont) is commercially dominating in the state-of-the-art PEMFCs. It is due to its high proton conductivity at moderate temperatures (<90 °C) and high chemical and mechanical stability. However, as Nafion is a perfluorinated sulfonic acid (PFSA) membrane, it suffers from several practical limitations such as high cost, hazard to the environment, relating to the fluorinated structure. At higher temperatures, it suffers low water retention owing to high degree of phase separation and consequently gas cross over, and a major performance reduction. In order to solve the issues, researchers all over the world considered and worked on different hydrocarbons as PEM. [5-9]. In this regard many research teams tried to replace Nafion with hydrocarbon-based membranes such as sulfonated poly(ether ether ketone), [10] sulfonated poly(fluorenyl ether ketone), [11] sulfonated poly(sulfone) [12] and sulfonated poly(arylene ether sulfone). [13]. Among these polymer membranes, sulfonated poly(ether ether ketone) (SPEEK) has been extensively investigated for the reasons such as easy sulfonation, high ion selectivity and low cost. [14],15]. The sulfonic acid groups in SPEEK proton exchange membranes are belonging to hydrophilic groups, which are generally affect the performance of the proton conductivity.[16] Attempts have been made to prevent the loss of water from the ionic pores of polymers by the way of membrane modification [17-19]. One such trial was incorporating hydrophilic metal oxide particles such as SiO<sub>2</sub> to enhance the water retention property and achieving proton conductivity under high temperature operating conditions. The previous effort in this regard also had some fruitful results [17,19,20].

The performance of PEMs are improved by the way of using an organic –inorganic composite membrane as it increases the water retention capacity and mechanical properties as well as reduced fuel permeation [21–24]. Wood/bio–based plastic composites is new avenue for researchers in the development of alternatives to conventional composites and petroleum-based materials. Wood plastic composites (WPC) promising the advantages such as waste management of natural products. This in turn has significant impact on environmental and economical interests, since the materials consume reduced energy in productions, and emit decreased volatile organic chemicals to the nature [25–27]. First requirement in order to make wood polymer composite is the polymer should be able to be processed at a low temperature[28]. PEMFC operates in this range, so that have made a maiden effort to make SPEEK wood powder ( *Azadirachta indica* ) composite membrane for PEM applications.

## II. EXPERIMENTAL

### A. Materials

The PEEK powder (150XF) was purchased from Victrex (England) with purity of 99.9% was used as received. Sulphuric acid (H<sub>2</sub>SO<sub>4</sub>) and 1-Methyl-2-pyrrolidone (NMP) both of AR grades supplied by E-Merck india Ltd. were used as received. The cost effective materials for fabricating a test fuelcell were purchased from Sainergy Fuelcell India Pvt Ltd (Such as Carbon Vulcan XC-72, Carbon Cloth and 40% Pt in Vulcan XC-72). In addition, a 60% Teflon dispersion purchased from Sigma Aldrich, USA and Isopropyl Alcohol (IPA- AR grade) was purchased from Rankem Chemicals for fabrication were used as received for fabrication

### B. Preparation of SPEEK/AI Composite Membranes

- 1) *Sulphonation of PEEK*: A known quantity of PEEK powder was taken in a round bottom flask which was mixed with 150ml H<sub>2</sub>SO<sub>4</sub> and stirred continuously for 6 hours using magnetic stirrer. The sulphonation reaction was arrested in an ice bath. [29,30]. The resulting Sulphonated PEEK (SPEEK) fibres were washed in double distilled water to have neutral pH and later dried for 3 hours in hot air oven at 60°C.

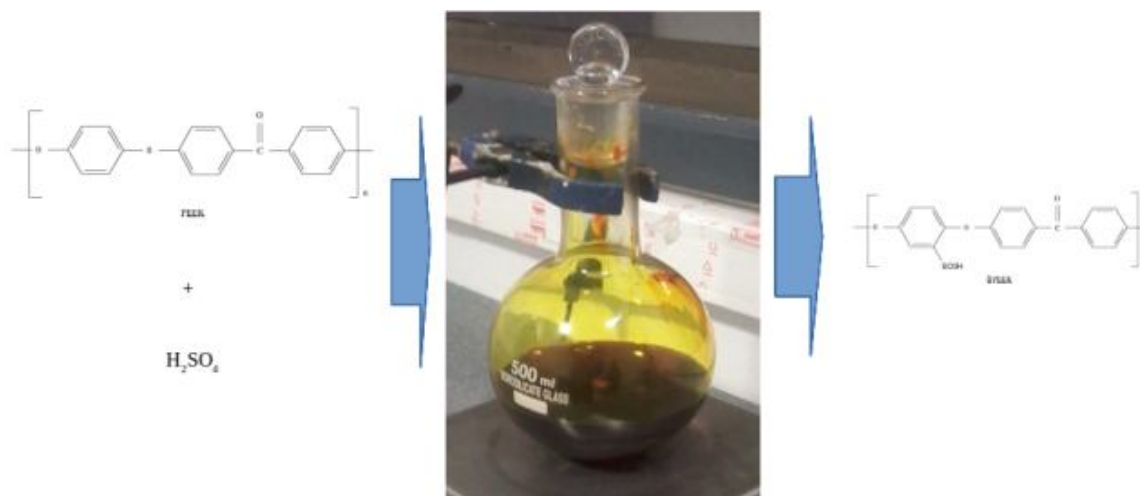


Fig.1 Sulphonation of PEEK.

- 2) *Preparation of Azadirachta indica Wood Powder (AI)*: Heartwood nucleus of AI wood powder was collected from the available source and was shallow dried for 24 hours and subsequently dried in hot air oven at 60°C so as to remove certain moisture present. Later the AI wood powder was made into a coagulated paste formation using deionised water as a solvent. As prepared paste like AI wood powder conserved in a petri dish placed in an hot air oven as it was placed earlier for the same 24 hour duration. The resultant product furtherance made into finassy using a pistle/mortor setup and this time it was kept in oven for 48 hours at 60°C.
- 3) *Preparation of SPEEK/AI Composite Membrane*
  - a) *Step1 Process*: The SPEEK was dissolved in NMP at ambient temperature and the mixture was stirred continuously for an hour. The homogenous solution so obtained was then filtered and cast on to a dry and clean petri dish. The petri dish was so filled kept in an oven at 60°C for 24hours. The membranes so prepared in this process were found to be pale brown in colour as shown.

b) *Step2 Process:* The measured quantity of AI was dispersed in NMP and the solution was stirred for 2 hours. The AI dispersion so prepared was then added in drop by drop into the SPEEK NMP Binary solution and the resulting ternary mixture was stirred for 4 hours till it turned into homogeneity. This homogeneous solution was cast onto a clean petri dish and dried in the hot air oven at 60°C for slow evaporation of the solvent to avoid any fissures in the resulting membrane. After the complete evaporation, membranes were peeled off from the container and subsequently treated with 0.5N H<sub>2</sub>SO<sub>4</sub>, and washed with deionized water. A set of five different composites with varying concentrations of 99% SPEEK - 1% AI, 98% SPEEK-2% AI, 97% SPEEK-3% AI, 96% SPEEK-4% AI, 95% SPEEK- 5% AI, were prepared using the solvent casting technique. Thus prepared membranes were of 80-100 μm in thickness.

C. *Fabrication of Membrane Electrode Assembly(MEA)*

The procedure for preparing a MEA adhered to standard protocols [1].

- 1) Purification of membrane.
- 2) Teflonization of porous carbon cloth
- 3) Carbonization of the teflonized carbon cloth
- 4) Catalyst layer first stage coating
- 5) Catalyst layer second stage coating
- 6) Hot pressing of the electrodes on the membrane

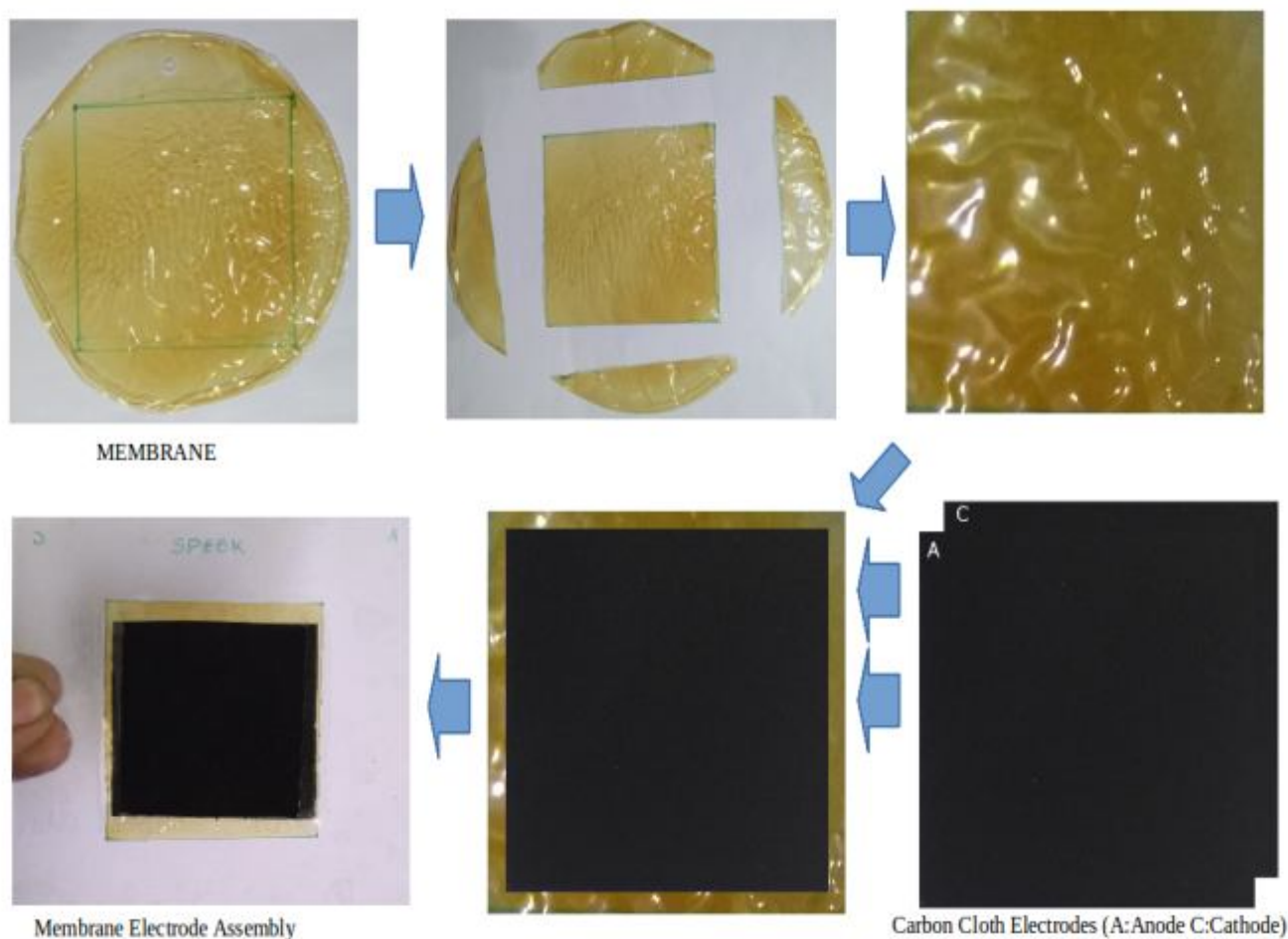


Fig.2 MEA Preparation stages

1) *Purification of the membrane:* Purification of the membrane is very crucial and must be performed before the preparation of MEA. Initially, all membranes were allowed to boil in 3% H<sub>2</sub>O<sub>2</sub> for 45 minutes which removed the impurities, if any, present

on the surface of the membrane. It was then washed thoroughly with distilled water and boiled for 30 minutes in 10% H<sub>2</sub>SO<sub>4</sub> to remove any inorganic impurities and to get the membrane in a complete protonated form. Finally, the membrane was washed with boiling water to remove any excess acid present on the surface of the membrane and later the membrane was dried.

- 2) *Teflonization Of The Porous Carbon Cloth:* For the teflonization process, a 60% Teflon dispersion in water available commercially was procured and was further diluted with deionised water in the ratio of 1:5. The carbon cloth was highly porous in nature and was dipped in the above dispersion for 30 seconds. Then soaked carbon cloth was placed in a muffle furnace at 350°C for 3 hours. The process of teflonization improve the hydrophobicity of the carbon cloth.
- 3) *Carbonization of the teflonized carbon cloth:* This is also called as the Gas Diffusion Layer (GDL). Initially Vulcan XC-72 (3mg/cm<sup>2</sup>) is mixed with 3ml of deionised water and sonicated for 10 minutes. The sonication was done to obtain a fine dispersion of the carbon particles. Then 2-3 ml of isopropyl alcohol was added and sonicated again for 10 minutes. Finally, a drop of Teflon dispersion was added, mixed and immediately coated on the carbon cloth by means of a brush. The cloth was then kept in a muffle furnace at 350°C for 3 hours.
- 4) *Catalyst Layer First Stage Coating:* The catalyst used was Pt dispersed in carbon. For the first stage, the amount of Pt taken was 0.125 mg/cm<sup>2</sup>. The required amount of the catalyst was weighed and mixed with 3 ml of water and sonicated for 10 minutes. Then few drops of Iso Propyl Alcohol (IPA) was added and sonicated for another 10 minutes. Finally, one drop of Teflon dispersion was added, mixed with the help of a painting brush and coated immediately on the carbonized cloth. It was then heated in a muffle furnace at 350°C for 3 hours.
- 5) *Catalyst layer Second Stage Coating*
  - a) *Anode:* For the second stage, the amount of Pt taken was 0.125 mg/cm<sup>2</sup>. The required amount of the catalyst was weighed and mixed with 3 ml of water and sonicated for 10 minutes. Then few drops of SPEEK solution was added and then coated immediately on the carbon cloth over the catalyst layer coated during the first stage. It was then dried in a hot air oven at 80°C for 4 hours. The electrode obtained after drying could be used as the anode for the fabrication of the MEA.
  - b) *Cathode:* For the second stage, the amount of Pt taken was 0.375 mg/cm<sup>2</sup>. The required amount of the catalyst was weighed and mixed with 3 ml of water and sonicated for 10 minutes. Then 1-2 drops of SPEEK solution was added, mixed and coated immediately on the carbon cloth over the catalyst layer coated during the first stage. It was dried in an oven at 80°C for 4 hours. The electrode obtained was the cathode that could be used for the fabrication of the MEA.
- 6) *Hot pressing of The Electrodes on the Membrane:* On either side of the membrane, a solution of SPEEK in NMP was applied and the electrodes were placed on either side. It was hot pressed at 80°C for 45 seconds with a load of 0.5 tonnes. The two electrodes stuck onto the membrane after the hot pressing treatment. The resulting assembly was the Membrane Electrode Assembly. The above MEA was used in the PEMFC for performance evaluation.

#### D. Characterizations

- 1) *Membrane Characterization:* XRD measurements were performed using an Ultimate IV diffractometer of Rigaku, Japan. The dried samples were mounted on an aluminium sample holder. The scanning angle ranged from 10° to 80° at a scanning rate of 2° per min. All the spectra were taken at ambient temperatures (25 ± 2°C). The IR spectra for the dried membranes were recorded with a Perkin Elmer / Spectrum 2 Diamond UATR FT-IR spectrometer for wave number 400 – 4000 cm<sup>-1</sup>. The samples were dried at 100°C for an hour before recording the spectrum. TGA analysis was mainly carried out to determine the thermal stability of the composite membranes. The change in weight of the membrane with increase in temperature at a heating rate of 10°C/min in the range of the temperature between 30°C and 750°C was followed using a Thermo Gravimetric Analyzer SDT Q600 of TA Instruments, USA. All the runs were carried out under nitrogen atmosphere. The surface morphology of the electrolyte membranes was analysed using SEM (Hitachi S – 3400 N). The samples were cut into sufficient size and sputter coated with gold to make the samples electro conductive. The samples were then analyzed under vacuum condition at an accelerating voltage of 10 KV. The amount of solvent intake by the membranes was studied. The dried membranes were weighed and soaked in water and methanol separately and allowed to get equilibrated at room temperature for 40 hours, above which the weight was constant. The swollen membranes were then immediately weighed after blotting the surface water and the values noted. The swelling degree was determined using the formula,

$$SW = \frac{M_{wet} - M_{dry}}{M_{dry}}$$

where,

M wet = Weight of wet membrane,

M dry = Weight of dry membrane

- 2) *Ion exchange capacity (IEC)*: The ion exchange capacity (IEC) indicates the number of mill equivalents of ions in 1g of the dry polymer. It was determined by titration method. The membrane in its protonated form was weighed and then soaked in an aqueous solution containing a large excess of KCl in order to extract all the protons from the membrane. The electrolyte solution was then neutralized using a very dilute Na<sub>2</sub>CO<sub>3</sub> solution of known concentration (0.01N). The EW (equivalent weight) values were calculated from the dry weight of the membrane divided by the volume and the normality of the Na<sub>2</sub>CO<sub>3</sub> solution. The IEC values were expressed as number of meq. of sulphonic groups per gram of dry polymer.

IEC is calculated using the formula,

$$IEC = \frac{\text{Titer value (in ml)} \times \text{Normality of the titrant (Na}_2\text{CO}_3)}{\text{Weight of the dry polymer membrane (in grams)}}$$

- 3) *Proton Conductivity*: The proton conductivity measurements were taken using an alternating current impedance spectroscopy device over a frequency range of 1-10<sup>7</sup> Hz with 50 - 500mV oscillating voltage using a Hioki 3532-50 LCR HiTester. Films having 1cm<sup>2</sup>, sandwiched between two stainless steel block electrodes with ~3 kg/cm<sup>2</sup> pressure, were placed in an open, temperature-controlled cell. The films were previously hydrated by soaking in deionised water for 24 hours at room temperature. The conductivity σ of samples were calculated in the transverse direction from the impedance data, using the relationship

$$\sigma = \frac{d}{RS}$$

where, d and S are the thickness and face area of the membrane sample, respectively, and derived from the low intersection of the high frequency semi-circle on a complex impedance plane with the Re(Z) axis. The impedance data were corrected for the contribution from empty and short circuited cell.

- 4) *Oxidative Stability*: For checking the durability of the electrolyte membranes, the following procedure was adopted. Initially a 4ppm ferrous ammonium sulfate in 3% H<sub>2</sub>O<sub>2</sub> was freshly prepared and the temperature of the solution was maintained at 80°C. The electrolyte membrane with the dimension of 0.5cm<sup>2</sup> was cut and soaked in the solution. The time required for the physical disintegration of the membrane was noted down and reported. The reaction is expected to occur by free radical mechanism.
- 5) *Single Cell Fuelcell performance Test Performance Evaluation*: Selected sample was subjected to testing in real time PEMFC environment with hydrogen gas as fuel with fabricated fuelcell at Amrita Lab, Coimbatore. Standard fuel cell grade graphite plates and copper current collectors were used for this purpose. The output voltage and the current were measured with a digital multimeter (CD800a of Sanwa, Japan with accuracy of ±0.7% with resolution of 0.1mV) under different resistances as loads.

### III.RESULTS AND DISCUSSION XRD STUDIES

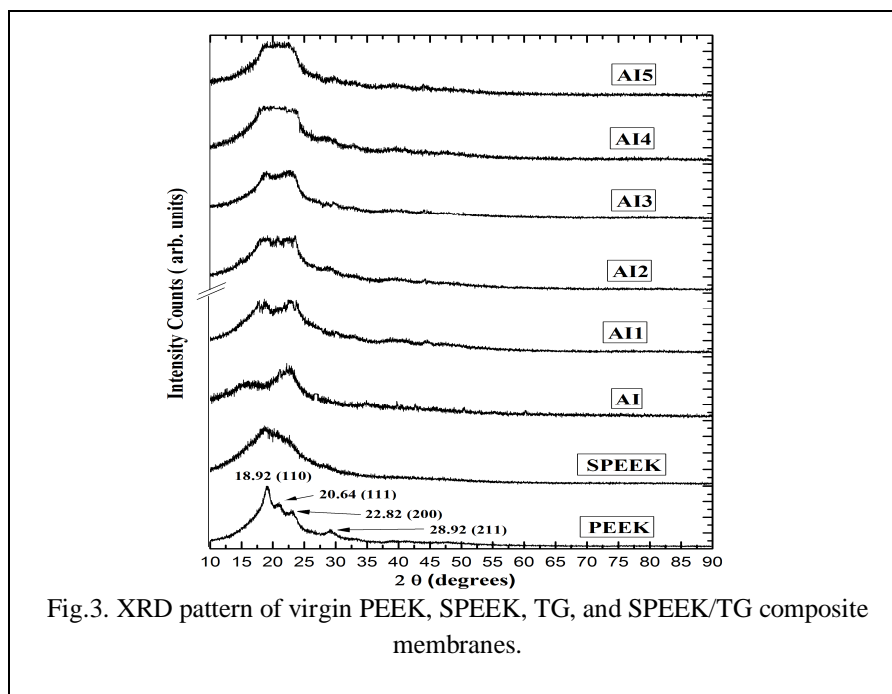


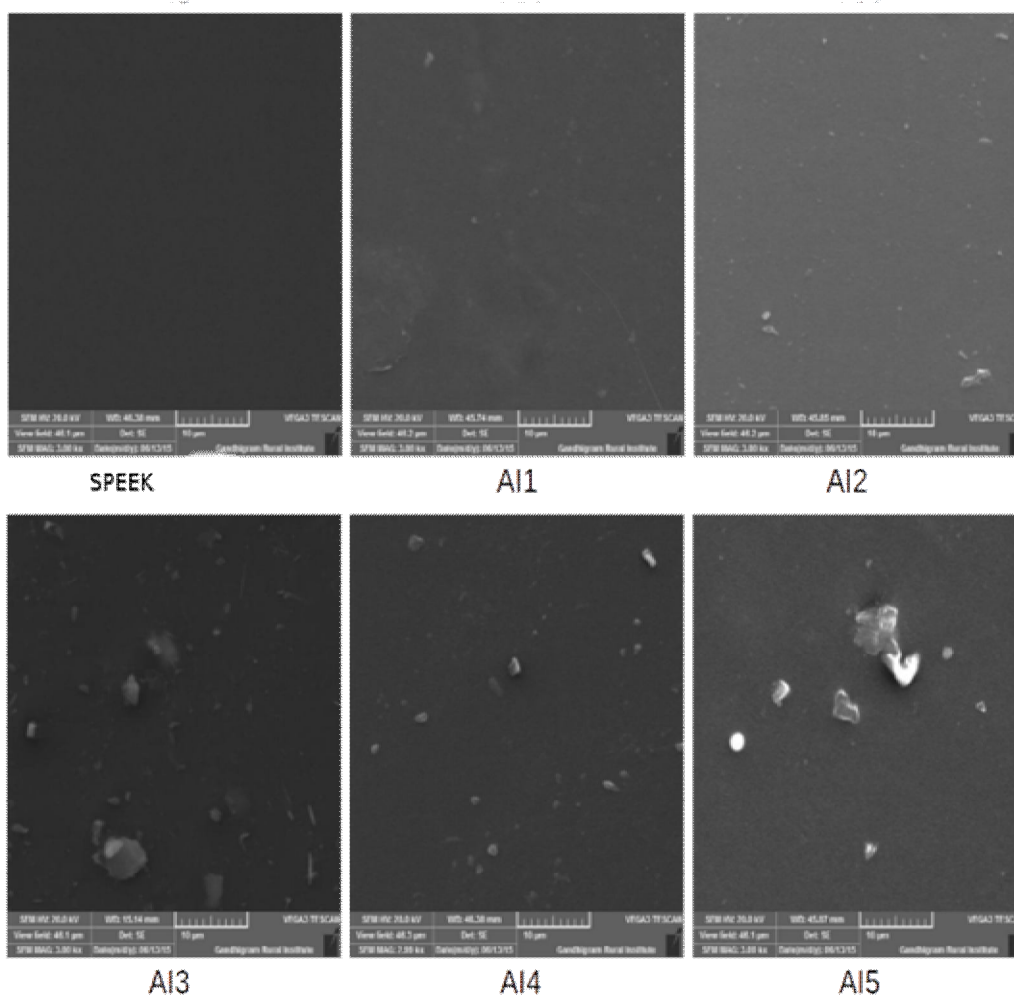
Fig.3. XRD pattern of virgin PEEK, SPEEK, TG, and SPEEK/TG composite membranes.

### A. XRD Studies

The XRD pattern of PEEK, SPEEK, AI and various composites of different membranes are shown in fig3. PEEK shows XRD peaks at 18.9°, 20.6°, 22.8° and 28.9° due to its semi-crystalline nature. These peaks can be ascribed to the diffraction at (110), (111), (200) and (211) crystalline planes of PEEK, respectively. Introduction of SO<sub>3</sub>H group reduces the crystallinity of PEEK due to restriction imparted by functional groups in ordered packing of polymeric chains. Thus intensity of (110) peak is reduced in SPEEK accompanying with relative broadening. Other crystalline peaks are not observed in SPEEK due to disruption of crystalline structure and becomes amorphous. [31,32] Diffraction peaks at 16.0° and 22.5° appear in the wood spectra, which originated from the crystalline region of the cellulose in the wood. [33] The broadness of the humps implies the amorphousity in teak saw dust[34]. In the case of composite membranes the above said peak slowly diminishes and a new broadened bump develops between 17° and 22°. Both together broadened the peak and the blended membrane become amorphous. In composite membranes, absence of this peak indicate an increase in the amorphous nature. This results a more flexible membrane apt for PEMFC application with better life.

### B. SEM Studies

The SEM images of virgin SPEEK and SPEEK+AI composite membranes are given in fig4. All the SEM images look dense, clear and homogenous indicating a uniform distribution of Azadirachta indica in the polymer matrix. No fissures could be observed in the virgin as well as composite membranes. This is due to the use of high boiling point solvent used for casting purpose. During the membrane formation, the solvent is evaporated at a very slow rate so that the continuity of the polymer matrix is maintained. The solvent is evaporated at a temperature of 80°C even though the boiling point of the solvent is 202°C.



**C. FTIR Studies**

Fig.1 shows the comparative FTIR spectra of PEEK, SPEEK and the various composite membranes. The peak observed at  $1485\text{ cm}^{-1}$  in PEEK is the aromatic C-C band, which was split into  $1490$  and  $1472\text{ cm}^{-1}$  in SPEEK due to the new substitution from the sulphonation reaction. The new peaks observed at  $1024$  and  $1080\text{ cm}^{-1}$  correspond to symmetric and asymmetric stretching vibration of the sulfonic acid group in SPEEK.[35,36] There is a significant broad peak at  $3460\text{ cm}^{-1}$  in SPEEK is assigned to OH vibration from sulphonic acid groups interacting with molecular water[37]. In the SPEEK composite membranes, the hydroxyl band is observed at  $3460\text{ cm}^{-1}$ , with a small shift in wavelength attributes to the effective hydrogen bonding interactions between SPEEK and the filler.[1]. Here it is observed in OH broad peak. It is already reported by Dogan et al. [38] that most of the characteristic peaks of the filler are blocked due to the interference by the SPEEK matrix even though in the highest percentages. In our FTIR spectrum of the PEEK/AI blend membranes also observed the same. The peak between  $1600\text{ cm}^{-1}$  and  $1750\text{ cm}^{-1}$  are due to the vibration of carbonyl group of SPEEK.

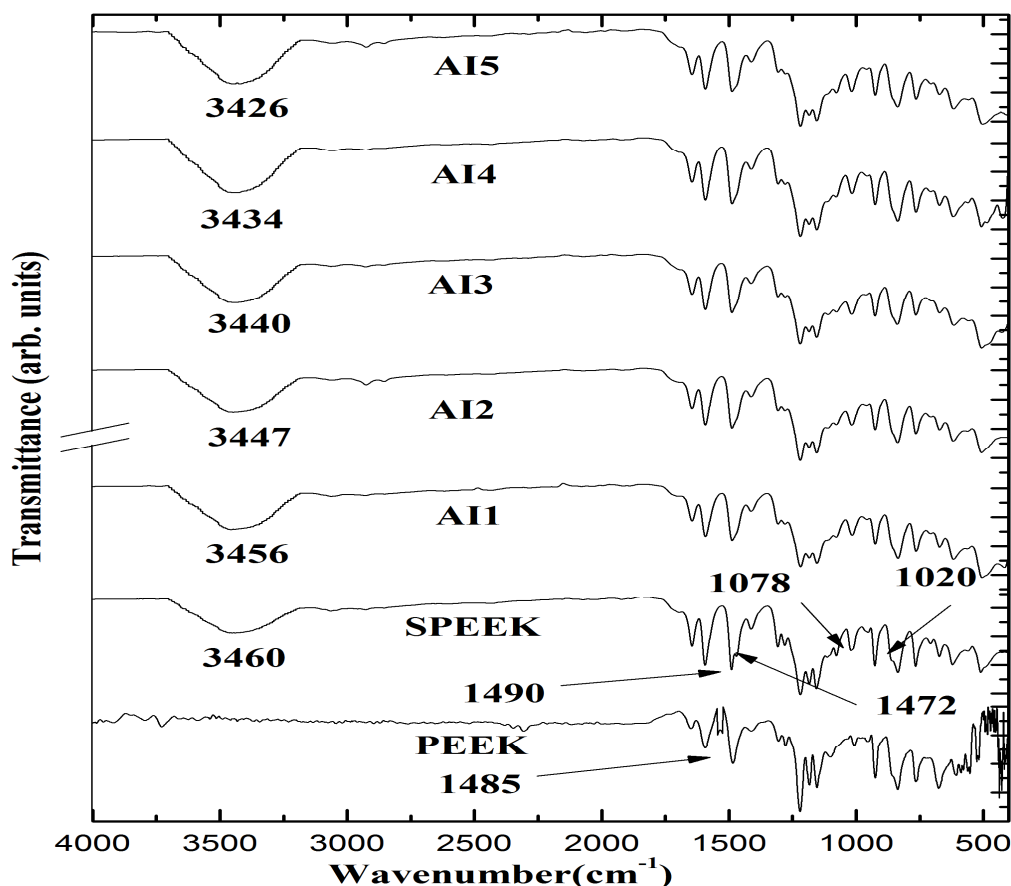


Fig.5.FTIR spectra of PEEK, SPEEK and SPEEK/TG composites

**D. TGA Studies**

The thermogram of SPEEK and various composite membranes are shown in fig.6. The thermogram of the composite membranes are found to be similar to that of SPEEK. A three stage degradation is observed for the electrolyte membranes. The first weight loss is observed between  $80^{\circ}\text{C}$  and  $150^{\circ}\text{C}$ . This weight loss may be attributed to the loss of physically and chemically adsorbed water. Even though the composite membranes exhibit a better water absorption capacity, the thermal energy available at temperatures over  $120^{\circ}\text{C}$  is sufficient to break the interaction between water and wood material and there by liberates water. However the weightloss extends up to  $150^{\circ}\text{C}$ . The second major weight loss is between  $230^{\circ}\text{C}$  and  $350^{\circ}\text{C}$ . This may be reasoned be due to the liberation of sulphonic acid group attached with the polymer matrix. The third loss is found between  $425^{\circ}\text{C}$  and  $600^{\circ}\text{C}$  may be attributed to the degradation of the polymer matrix.

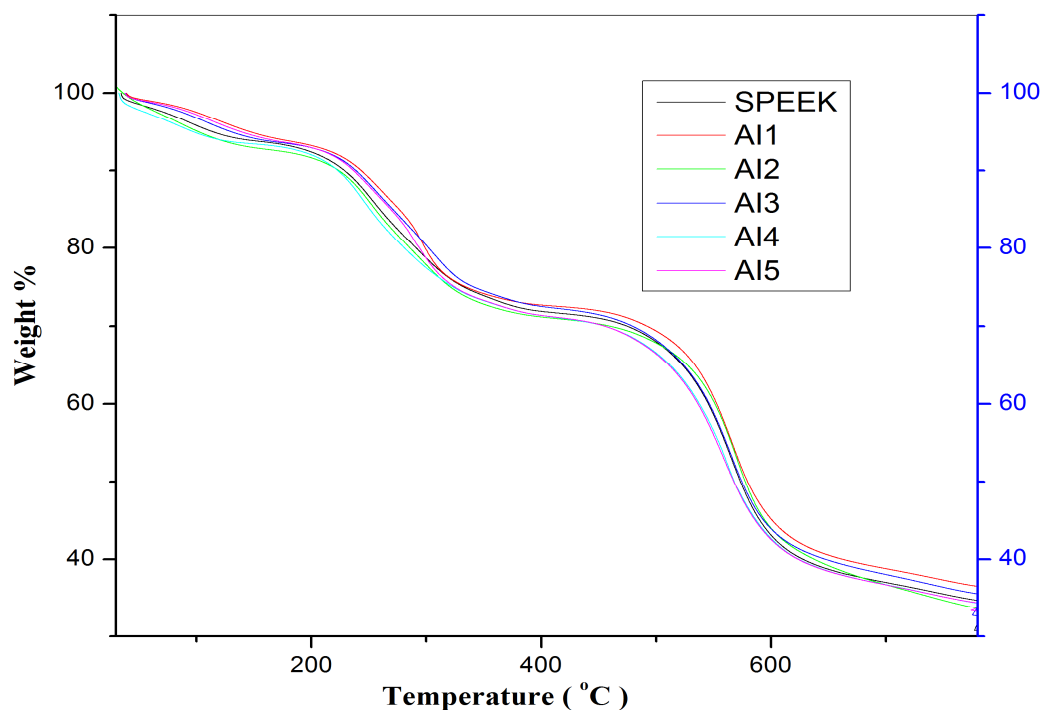


Fig.6. TGA of Virgin SPEEK and SPEEK/TG composite membranes.

*E. Ion Exchange Capacity*

The Ion- Exchange Capacity of pure SPEEK and SPEEK/*Tectona grandis* membranes are given in table 1. It is observed that IEC of pure SPEEK is found to be 2.17 meq/g, and it might be due to the loading of *Azadirachta indica* which could enhance the magnitude of IEC. Consequently, the enhancement of IEC is found to be increased gradually with increase in concentration of *Azadirachta indica*. This increasing trend may be due to the significant water absorbing capacity of the *Azadirachta indica*. Before observing the role of organic content in the composite membrane, it was presumed that increase in organic content in the composite membrane would decrease the magnitude of IEC. But, it showed reverse trend, in empirical observations, that IEC magnitude started to increase with increase of it.

TABLE I  
OBSERVED RESULTS OF THE MEMBRANES

Sample	Test Values			
	IEC meq/g	Water Absorption wt%	Chemical Stability min	Protonic Conductivity mS/cm
SPEEK	2.16	14.18	255	8.51
AI1	2.18	15.24	251	8.70
AI2	2.21	16.39	249	8.97
AI3	2.26	17.41	243	9.19
AI4	2.28	18.49	239	9.49
AI5	2.30	19.60	231	9.71

### F. Water Absorption

The Table 1 Presents water absorption (wt%), chemical stability of samples pristine SPEEK and its composites. It is noted that the water absorption of SPEEK is found to be 14.18 wt% whereas it is 19.60 wt% against the sample AI5 wherein the maximum concentration of Azadirachta indica is present. This suggests that the water absorbing capacity is found to vary as a function of the concentration of Azadirachta indica. The hydrophilic sulphonic acid group is mainly responsible for the water absorption. With increase in the content of wood powder, the net content of sulphonic acid group decreases, even then there is increase in the water absorbing ability. This may be due to the greater water absorbing capacity of the wood powder.

### G. Proton Conductivity

The proton conductivity of SPEEK with various concentration of Azadirachta indica is given in the fig.7 The sulphonic acid group available in SPEEK is primarily responsible for the transportation of protons. The proton conductivity of the composite membranes are found to be in an increasing trend when compared to SPEEK. This clearly shows that the composite membranes are capable of transporting protons better than virgin SPEEK even though there is a decrease in the net sulphonic acid group with increase in the wood content. This peculiar nature may be due to the increased water holding capacity of the composite membranes as compared to SPEEK.

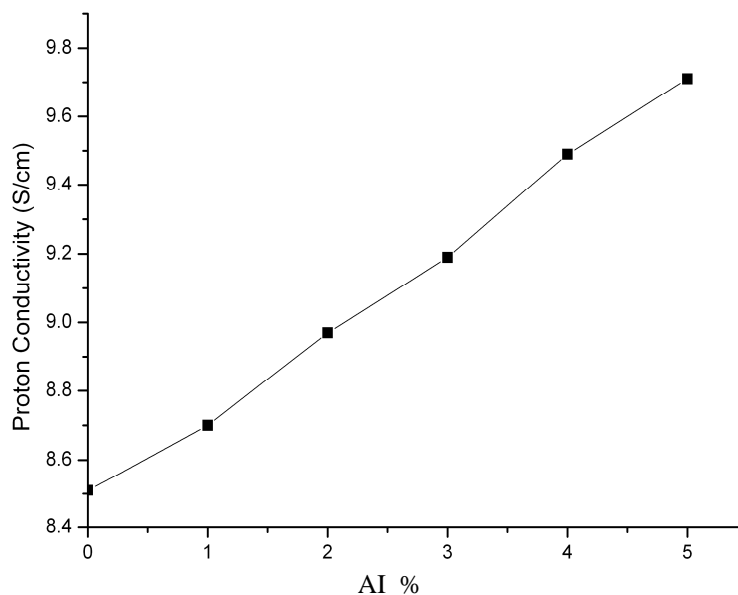


Fig. 7. Proton conductivity at various AI concentrations

### H. Chemical Stability

The experimental results of hydrolytic stability of various electrolyte membranes were given in Table1. The hydrolytic stability of SPEEK is found to be 255 minutes. The oxidative stability of the composite membranes decreases with increase in the wood content. As we increase the composition of the wood content, the continuity in the polymer matrix is disturbed and hence there can be regions where breaking is relatively easy. This may be the reason for the decrease in the hydrolytic stability of the composite membranes.

### I. Single cell Performance

The prepared pure SPEEK and SPEEK-AI membranes are subjected to single-cell test in order to evaluate their suitability for fuel cell applications. Figure 8 displays the single-cell performance of fabricated composite membrane at room temperature 30 °C. The open circuit voltage for the composite is observed to be 0.924V comparing to that of pure SPEEK at 0.896V. The peak power

density attained by SPEEK-AI composite is  $85 \text{ mWcm}^{-2}$ , which is comparatively higher than that of Pure SPEEK ( $76 \text{ mWcm}^{-2}$ ). This result indicates that the prepared membrane can be used as potential candidate for PEMFC.

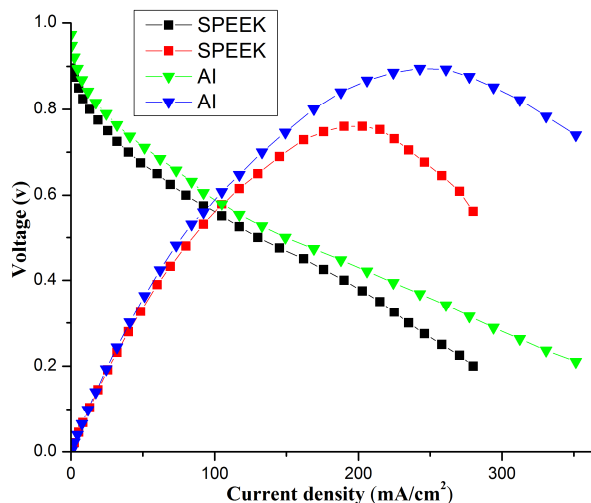


Fig.8 Single cell performance studies for virgin SPEEK and SPEEK/AI composite membranes

#### IV. CONCLUSIONS

From the results documented as above it is concluded that SPEEK-AI composite membranes are excellent candidates as electrolyte membranes for fuel cell applications owing to the high stability, improved proton conductivity and appreciable thermal stability. From the various studies it is observed that the composite membrane labelled as AI-5 is found to be ideal for fuel cell application. The performance of the above said membrane is also studied and found to be on par with the commercial membranes.

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