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Abstract: India is the third larger producer of fruits and vegetables in the world. These products are planning mainly for domestic consumption and sale in the local area market. However, in case of surplus production, enormous losses occur because farmers neither have access to markets in big cities nor to the international market due to poor product quality and market reach. As another to the marketing of fresh fruits and vegetables, small farmers can think of conservation by drying. Drying is an essential process in the conservation of agricultural crops, wastewater treatment, and biomass treatment.

I. INTRODUCTION

The energy requirement for drying can be supplied from various sources, namely, fossil fuel, natural gas, electricity, wood, bark forest remaining, and solar. Although the use of solar radiation for drying has existed since a long ago times, it has not yet been widely commercialized, particularly in the agricultural sector. Considering the fast depletion of natural fuel resources and because of the rising fossil fuel cost, solar drying is expected to become indispensable in the future. Moreover, the main purpose of drying agricultural product is conservation, minimize storage and packaging spaces and make smaller weight for transportation and handling.

Solar drying is actually since the ancient time for preservation of food and agriculture crops. This was done particularly by open sun drying underneath open the sky. This process has several disadvantages like spoilage of product due to adverse climatic condition like rain, moist, wind and dust, loss of material due to birds and animals, failure of the material by decomposition, insects and fungus growth. Also the process is highly labor intensive, time consuming and requires large area. Thus solar drying is the best replacement as a solution of all the drawbacks of natural drying and unnatural mechanical drying. Solar dryers used in agriculture for food and crop drying.

II. DEVELOPMENT OF EXPERIMENTAL SETUP

A. Aspect to be Considered while Selecting the Dryer

For research work it is necessary to develop experimental test setup (system). The following points were considered in the design of the solar dryer system

- 1) The amount of moisture to be removed from a given quantity of wet leafy vegetables
- 2) Daily solar radiation to determine energy received by the dryer per day
- 3) The daily sunshine hours for the selection of the total drying time
- a) Heating Chamber: The heating chamber should have the following characteristics in order to increase the efficiency
- Should have an appropriate size for its projected use.
- Should be a convenient height.
- The floor and walls inside the drying chamber should be of a dark colour.
- b) Determining Optimum collector Slope: From the general knowledge of the apparent movement of the sun it can be seen that during the drying season the sun will be overhead at or near the tropic of Capricorn. Thus for a dryer situated in the northern hemisphere a south facing collector will receive most insolation. To calculate the optimum slope angle, taking March 15 as the midpoint of the drying season. Angle of declination δ is the angle made by the line joining centers of sun and the earth with the projection of this line on the equatorial plane. It arises by the virtue of the fact that the earth rotates about an axis which makes an angle of approximately 66.5° with the plane of its rotation around the sun. The declination angle varies from a maximum value of $+23.45^{\circ}$ on June 21 to a minimum value of -23.45° on December 21. δ is given by following relation



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$$\delta$$
 (in degrees) = 23.45 sin[$\frac{360}{365}$ (284 + n)]

Where n is the day of the year

For March 15, n = 74Hence δ (in degrees) = 23.45 sin

δ (in degrees) = 23.45 sin[$\frac{360}{365}$ (284 + 74)] = 23.45 sin[0.9863 (284 + 74)] $δ = -2.82^{0}$

But the angle of inclination (β) of collector for specific plane is generally taken as latitude plus 10 to 15 degrees. Therefore for Islampur,

Angle of latitude = 16.870

And angle of inclination (β) = 16.870+10

 $\beta = 26.870^{\circ}$

To maximize the level of insolation on a collector the simplest approach is to situate the collector so that it is perpendicular to insolation at mid-day in the middle of the dry season.

B. Performance Analysis of solar Tunnel Dryer

The performance of the dryer is evaluated by measuring the parameters like variation in moisture content, temperatures at various locations inside the drying chamber, Outdoor temperature variation, relative humidity, drying rate, drying time.

1) Moisture Determination

a) Dry basis:

The moisture content on dry basis (Md_o) of the leafy vegetable is expressed as

$$Md_{o} = \frac{W_{o} - W_{d}}{W_{d}} \times 100\%$$

The instantaneous moisture content of leafy vegetables on dry basis (Md_i) at any time (t_i) during the drying process is determined by following equation

$$Md_{i} = \frac{W_{i} - W_{d}}{W_{d}} \times 100\%$$
(2.3)

Where W_i is the weight of leafy vegetable at time t_i in kg.

b) Wet basis:

The moisture content on wet basis (Mw_o) of the leafy vegetable is expressed as

$$Mw_{o} = \frac{W_{o} - W_{d}}{W_{0}} \times 100\%$$
(2.4)

The instantaneous moisture content of leafy vegetables on wet basis (Mw_i) at any time (t_i) during the drying process is determined by following equation

$$Mw_{i} = \frac{W_{i} - W_{i}}{W_{o}} \times 100\%$$
(2.5)

Where W_i is the weight of leafy vegetable at time t_i in kg.

2) Drying Rate

The instantaneous drying rate DR_i is determined by using following equation

$$DR_{i} = \frac{\Delta W_{i}}{T_{d}}$$
Where,

 ΔW_i is the difference of weight between when two successive measurements of a drying material (leafy vegetables) is made.

(2.1)

(2.2)

(2.6)



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(2.7)

3) System Drying Efficiency (η_{d})

The system drying efficiency is defined as the ratio of the energy required to evaporate the moisture to the energy supplied to the dryer. For solar calculations the heat supplied to the dryer is the insolation upon the collector.

The system drying efficiency is calculated from the equation

$$\eta_{d} = \frac{\text{Amount of water removed from vegetable × HL}}{A_{c} × I_{i}} × 100\%$$
$$\eta_{d} = \frac{m_{W} - H_{L}}{A_{c} × I_{i}} × 100\%$$

Where.

 \mathbf{m}_{w} = Amount of moisture evaporated or removed (kg)

 $\mathbf{m}_{\mathbf{w}} = \mathbf{W}_{\mathbf{i-1}} - \mathbf{W}_{\mathbf{i}}$ where $\mathbf{W}_{\mathbf{i-1}}$ and $\mathbf{W}_{\mathbf{i}}$ are successive weight corresponding to when two successive measurements of a drying material is made.

 $\mathbf{H}_{\mathbf{L}}$ = Latent heat of vaporization of water, 2320 (kJ/kg)

 $\mathbf{A}_{\mathbf{c}} =$ Area of the collector (m²)

 \mathbf{I}_{i} = Instantaneous solar insolation upon collector

III.EXPERIMENTAL INVESTIGATION

Table 1 : Prototype dimensions used for testing solar tunnel dryer				
Sr. No.	Component	Particular	Value	
			(mm)	
		Length	1250	
1	Flat plate collector			
	-	Width	500	
		Thickness	3	
		Length	1250	
2	Evacuated type collector	Tube diameter		
		Tube Thickness	3	
		Length	1000	
2	Druor	Lengui	1000	
5	Diyei	Width	1000	
			590	
		Height	580	
		Length	700	
4	Dryer tray			
		Width	520	
		Height	50	
5	Glass cover thickness	-	6	

Table : Prototype dimensions used for testing solar tunnel dryer

IV.CONCLUSIONS

The purpose of drying agricultural products using solar tunnel dryer is to improve the quality of drying and preserve the products. The solar tunnel dryer has been designed and fabricated for drying leafy vegetables. The effects of different atmospheric conditions on the drying leafy vegetables are carefully observed. For the comparison performance of dryer following points are considered.Causal Productions permits the distribution and revision of these templates on the condition that Causal Productions is credited in the revised template as follows: "original version of this template was provided by courtesy of Causal Productions.



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	-			
Sr. No.	Particular	Air velocity		
		0.5 m/s	0.6 m/s	0.7 m/s
1	Final moisture content on			
	W.B. (%)	Fogging was	2.47%	3.04%
2	Total Drying time required	Occurred because the	3 hours 45 minute	4 hour
3	Maximum drying rate	air velocity	0.004 (kg/min)	0.003 (kg/min)
4	Average drying rate	was not sufficient	0.00197(kg/min)	0.0016(kg/min)
5	Average System drying	to Throughout the		
	efficiency	moist air	14.932%	13.48%

Table2: Result comparison of Evacuated tube type tunnel dryer for drying curry leaves

Table 2: Result comparison flat plate type solar tunnel dryer for drying curry leaves

Sr. No.	Particular	Air velocity		
		0.5 m/s	0.6 m/s	0.7 m/s
1	Final moisture content on			
	W.B. (%)	Fogging was	3.61%	3.75%
		Occurred because the		
2	Total Drying time required	air velocity	3 hours 45	4 hours 15 minutes
		was not sufficient	minutes	
		to Throughout the		
3	Maximum drying rate	moist air	0.004(kg/min)	0.0032(kg/min)
4	Average drying rate		0.0018(kg/min)	0.0015(kg/min)
5	Average System drying		15.02%	11 75%
	efficiency		15.0270	11.7570

Table3: Result comparison of Evacuated tube type tunnel dryer for drying fenugreek

Sr.	Particular	Air velocity			
No.		0.5 m/s	0.6 m/s	0.7 m/s	
1	Final moisture content on W.B. (%)				
		Fogging was	7.92%	8.12%	
2	Total Drying time required	Occurred because the air velocity	5 hours 30 minutes	6 hours 30 minutes	
3	Maximum drying rate	to Throughout the	0.0043(kg/min)	0.0040(kg/min)	
4	Average drying rate	moist air	0.00237(kg/min)	0.00196(kg/min)	
5	Average System drying efficiency		17.08%	14.96%	

Table4: Result comparison flat plate type solar tunnel dryer for drying fenugreek

Sr.	Particular	Air velocity		
No.		0.5 m/s	0.6 m/s	0.7 m/s
1	Final moisture content on W.B. (%)	Fogging was	8.22%	8.62%
2	Total Drying time required	Occurred because the air velocity was not sufficient to Throughout the moist air	5 hours 30 minutes	6 hours 30 minutes
3	Maximum drying rate		0.0041(kg/min)	0.0040(kg/min)
4	Average drying rate		0.0024(kg/min)	0.00199(kg/min)
5	Average System drying efficiency		17.035%	14.84%



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Sr. No.	Particular	Air velocity			
		0.5 m/s	0.6 m/s	0.7 m/s	
1	Final moisture content on W.B. (%)	Fogging was Occurred because the air velocity was not sufficient to Throughout the moist air	6.51%	6.21%	
2	Total Drying time required		5 hours 30 minutes	5 hours 45 minutes	
3	Maximum drying rate		to Throughout the	0.0048(kg/min)	0.0038(kg/min)
4	Average drying rate		0.0027(kg/min)	0.0021(kg/min)	
5	Average System drying efficiency		17.03%	20.01%	

Table 5: Result comparison of Evacuated tube type tunnel dryer for drying coriander

 Table 6: Result comparison flat plate type solar tunnel dryer for drying coriander

Particular	Air velocity		
	0.5 m/s	0.6 m/s	0.7 m/s
Final moisture content on			
W.B. (%)	Fogging was	6.71%	6.71%
	Occurred because the		
Total Drying time required	air velocity	5 hours 30	5 hours 45 minutes
	was not sufficient	minutes	
	to Throughout the		
Maximum drying rate	moist air	0.0040(kg/min)	0.0038(kg/min)
Average drying rate		0.0023(kg/min)	0.0022(kg/min)
Average System drying efficiency		16.89%	19.70%
	Particular Final moisture content on W.B. (%) Total Drying time required Maximum drying rate Average drying rate Average System drying efficiency	ParticularAir velocity0.5 m/sFinal moisture content on W.B. (%)Fogging was Occurred because the air velocity was not sufficient to Throughout the moist airMaximum drying rate Average drying ratemoist air	ParticularAir velocity0.5 m/s0.6 m/sFinal moisture content on W.B. (%)Fogging was Occurred because the air velocity

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